

Continuous CWPO reaction using new developed foam supported catalysts

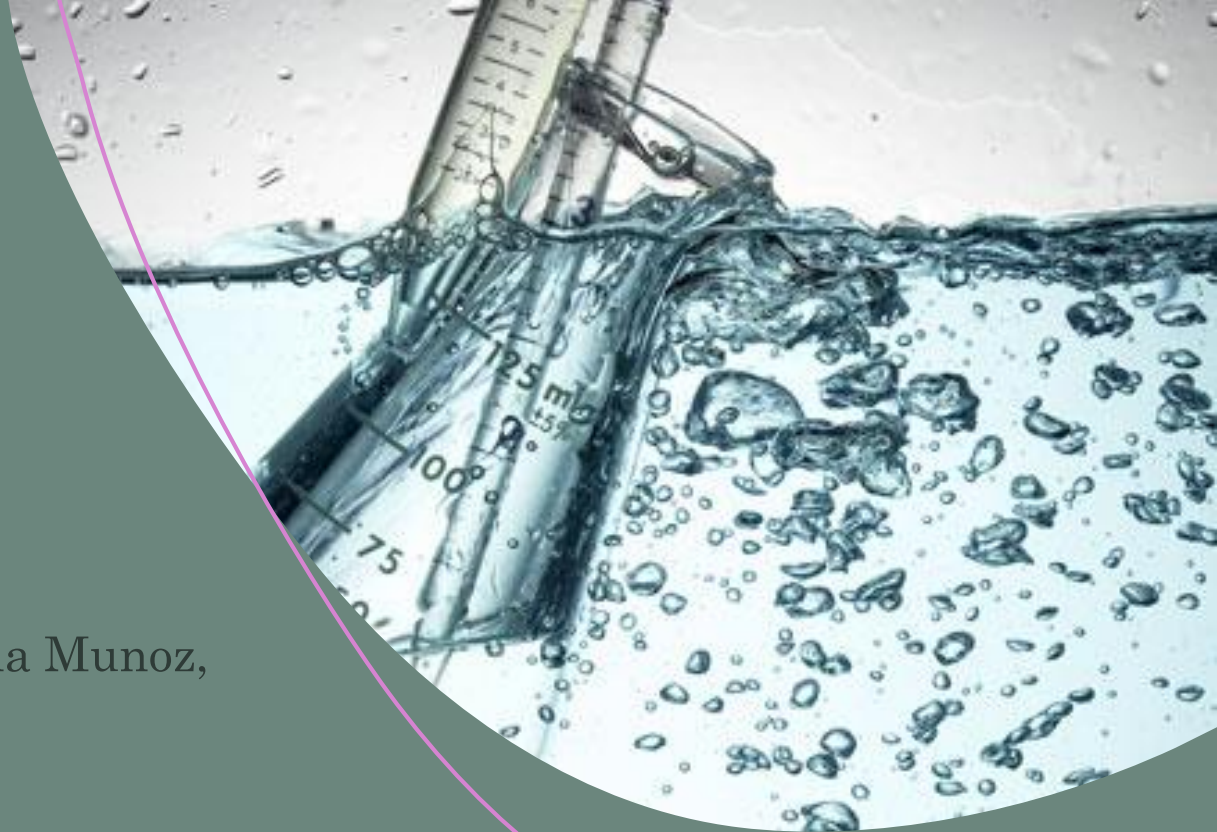
Esther Gomez-Herrero, Julia Nieto-Sandoval, Macarena Munoz, Zahara M. de Pedro, Jose A. Casas

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WORKSHOP REMTAVARES-BIOTRES

Diciembre 2020

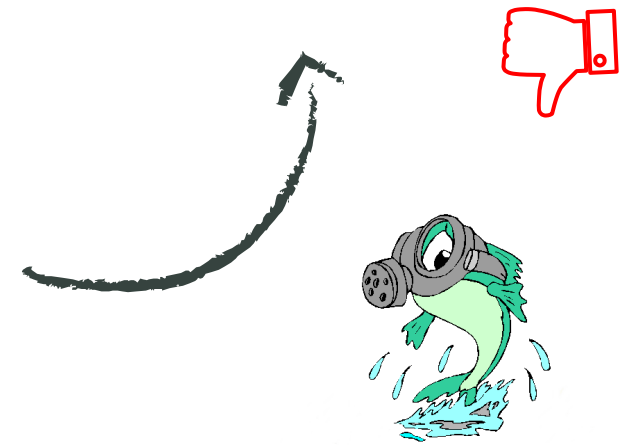
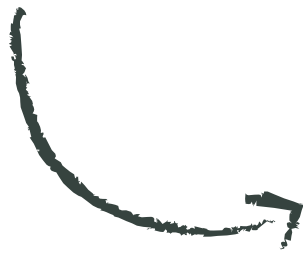
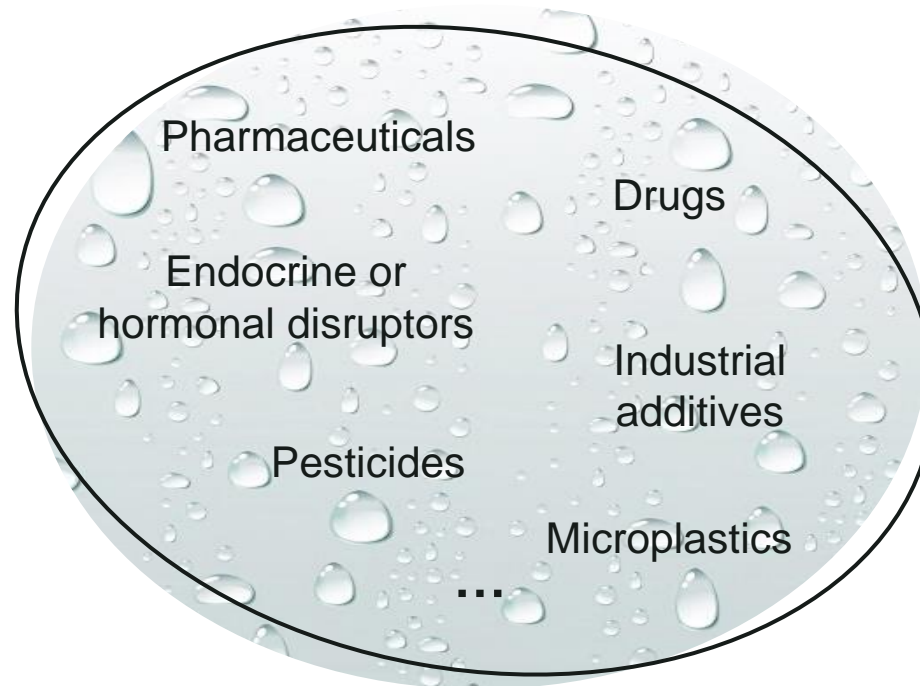
Innovative technologies for sustainable management of urban and industrial waste streams

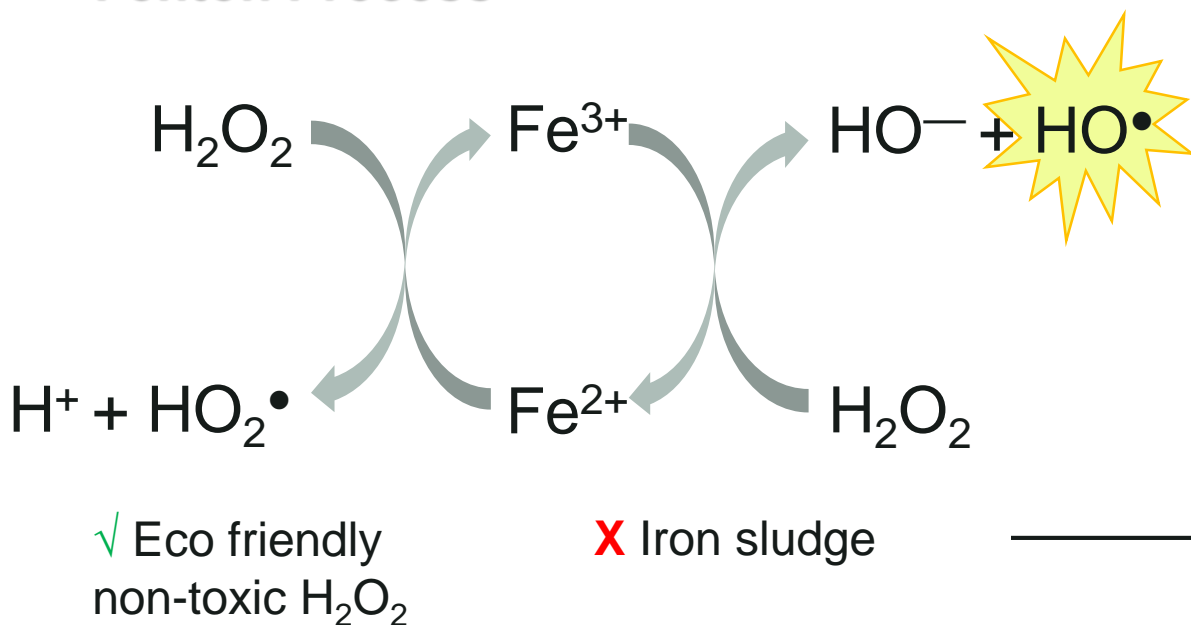
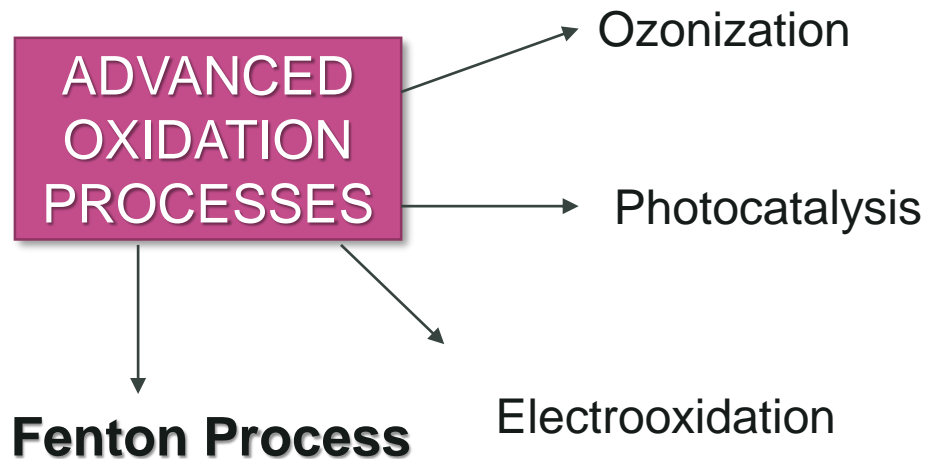




EMERGING POLLUTANTS

ngL⁻¹ — µgL⁻¹





Heterogeneous Fenton

Catalytic Wet Peroxide Oxidation **CWPO**

Powder catalysts

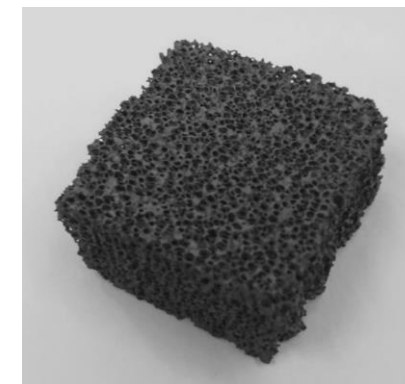


✓ Recovery

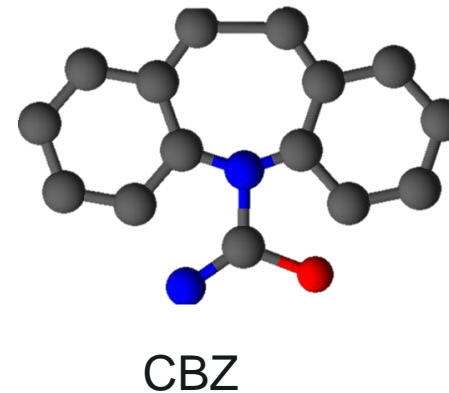
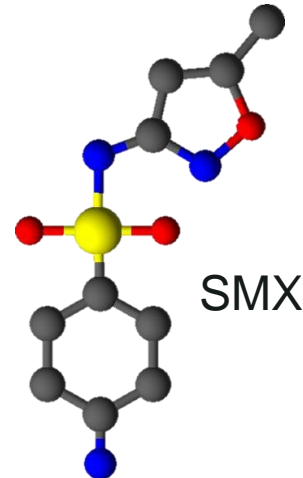
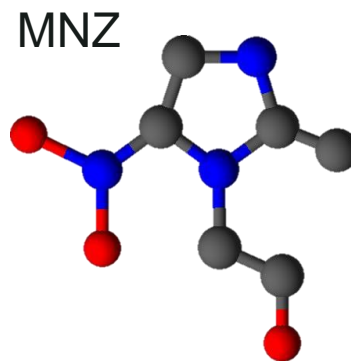
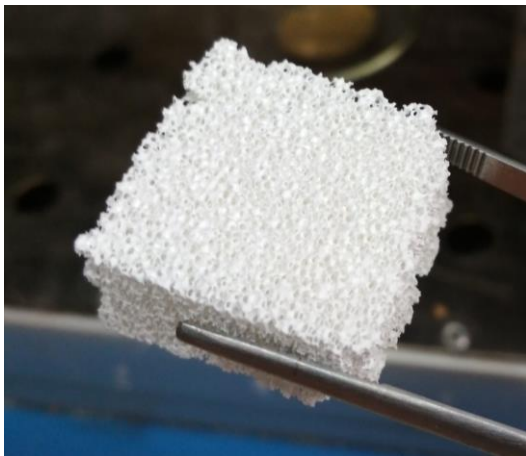
✗ Scale-up in continuous reactions

Structured catalysts

Open Cell
FOAMS



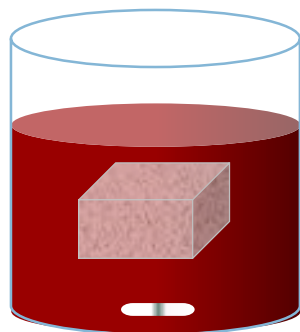
To develop homogeneous structured catalysts based on Al_2O_3 , SiC and ZrO_2 foam supports coated with an active phase of iron oxide. New catalysts were applied in the CWPO process for the removal of a mixture of pharmaceuticals in order to evaluate catalytic performance and stability and the effect of different operating conditions



Pharmaceuticals compounds concentration in wastewater

MNZ	1.8 $\mu\text{g L}^{-1}$
SMX	6.0 $\mu\text{g L}^{-1}$
CBZ	2.3 $\mu\text{g L}^{-1}$

ION ADSORPTION



30 min



10 min

Al_2O_3

SiC

ZrO_2

Fresh
support

Ion adsorption

Calcination

Reduction



CATALYSTS CHARACTERIZATION

Final catalysts appearance



Fe/Al₂O₃



Fe/SiC

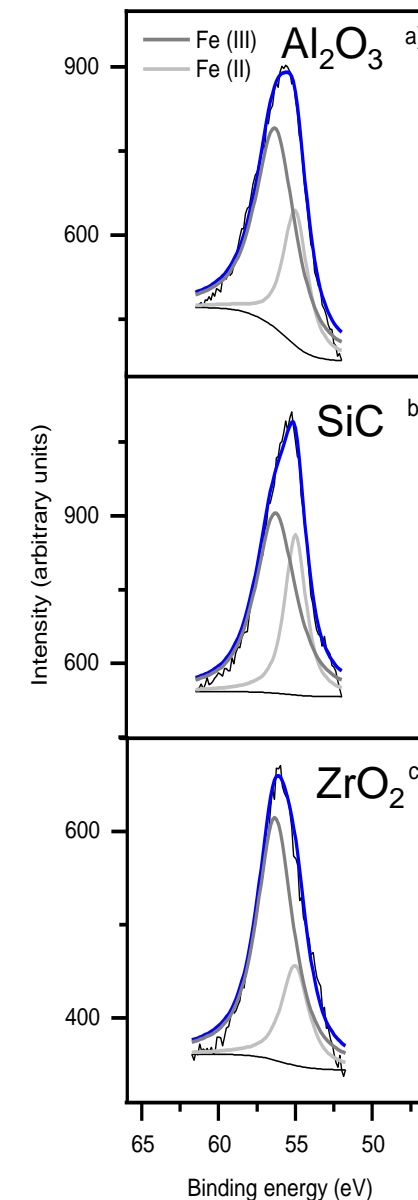
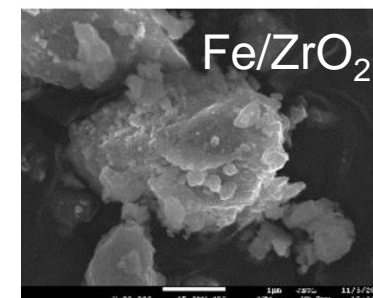
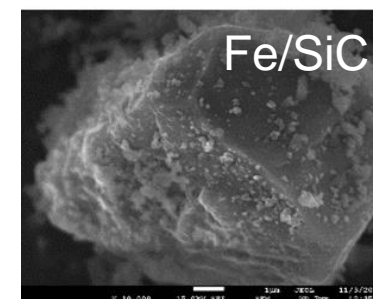
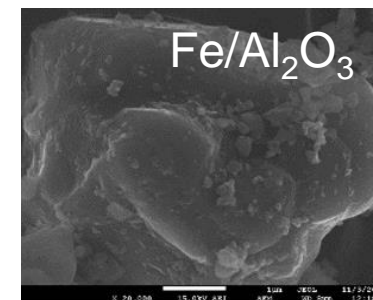


Fe/ZrO₂

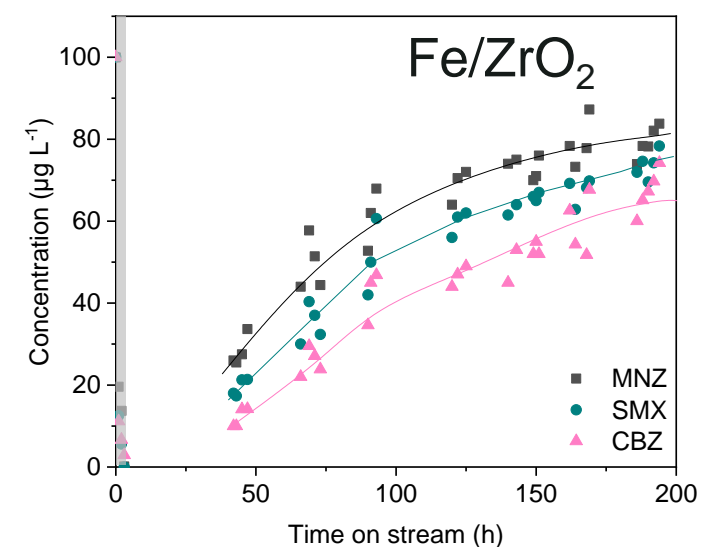
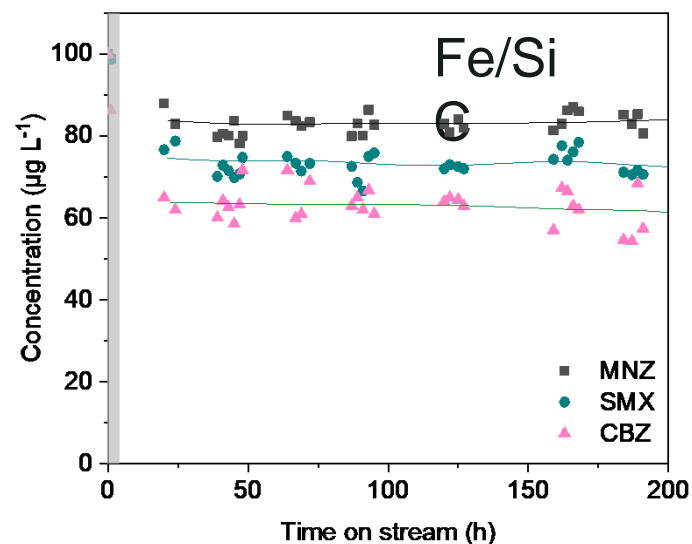
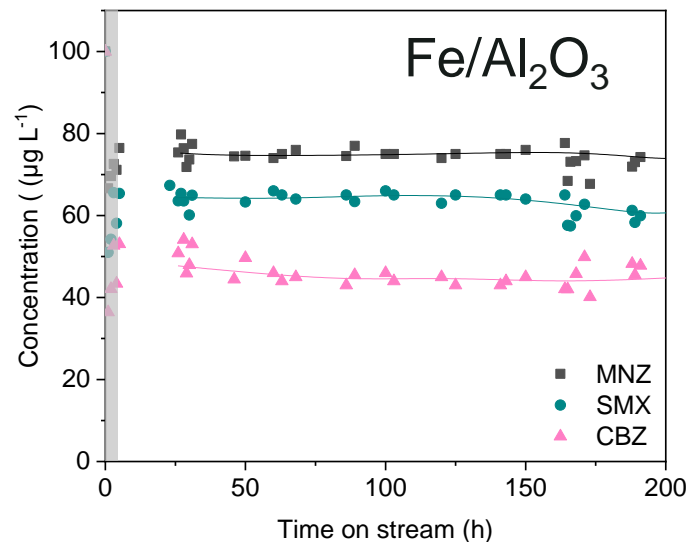
Low BET Surface area for all supports tested

	Fe load (%)	Nanoparticle size (nm)	XPS – ratio Fe(II) : Fe (III)
Fe/Al ₂ O ₃	2.50	100-200	0.30 : 0.70
Fe/SiC	2.12	100-200	0.32 : 0.68
Fe/ZrO ₂	0.90	150-400	0.24 : 0.76

↓
Magnetite
0.33 : 0.67



CATALYTIC ACTIVITY OF STRUCTURED CATALYSTS



Operating conditions:

$[MNZ, SMX, CBZ]_0 = 100 \mu\text{g L}^{-1}$

$[\%Fe\text{-foam}] = 0.9 - 2.5 \%$

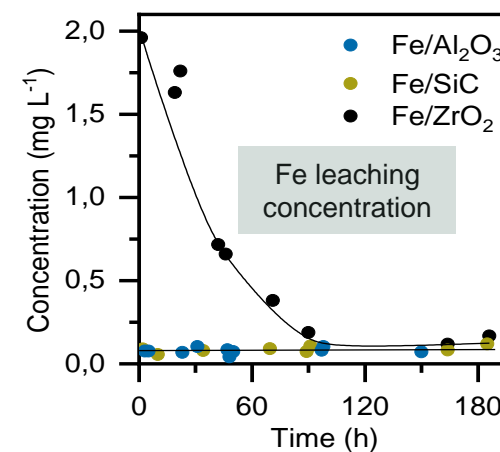
$H_2O_2 = 1,49 \text{ mg L}^{-1}$

$pH_0 = 5$

20°C

$Q = 1 \text{ mL min}^{-1}$

Conversion (%)	Fe/Al ₂ O ₃	Fe/SiC	Fe/ZrO ₂
MNZ	25	15	--
SMX	35	25	--
CBZ	50	40	--



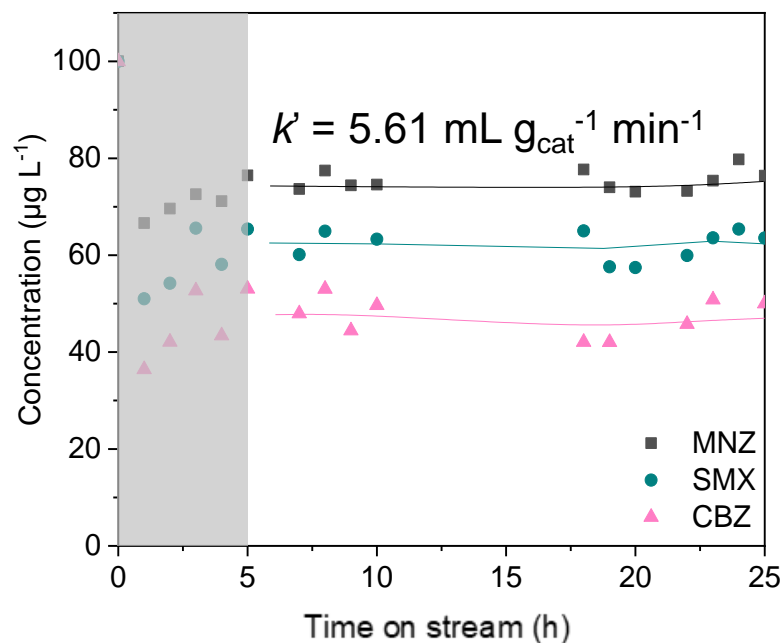
Fe load (%)	Prepared catalysts	Used catalysts
Fe/Al ₂ O ₃	2.5	2.2
Fe/SiC	2.1	2.0
Fe/ZrO ₂	0.9	0.5



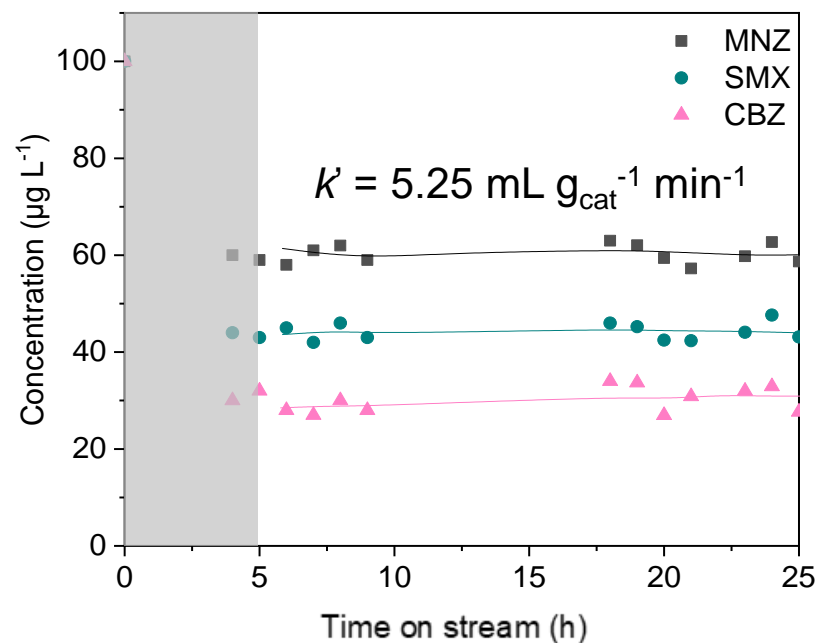
EFFECT FLOW RATE – Fe/Al₂O₃

foam

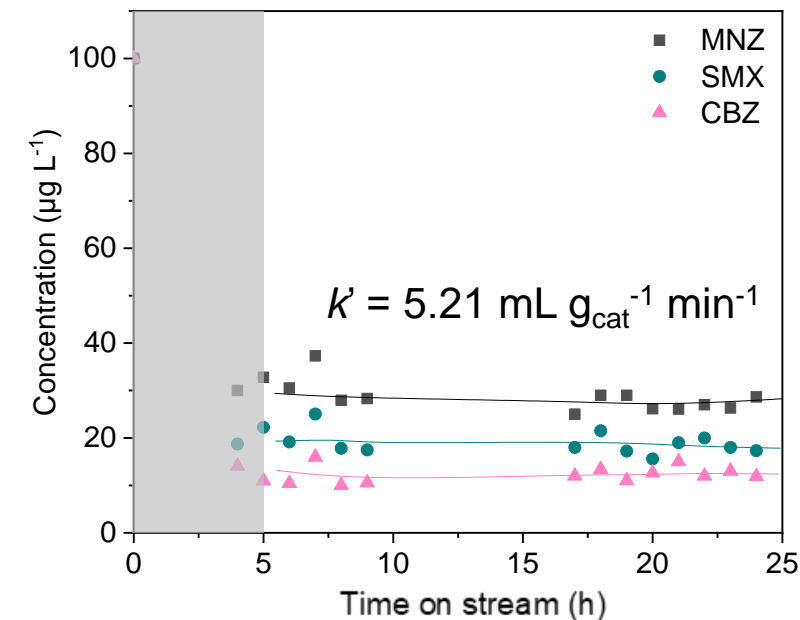
Q = 1 mL min⁻¹



Q = 0.5 mL min⁻¹



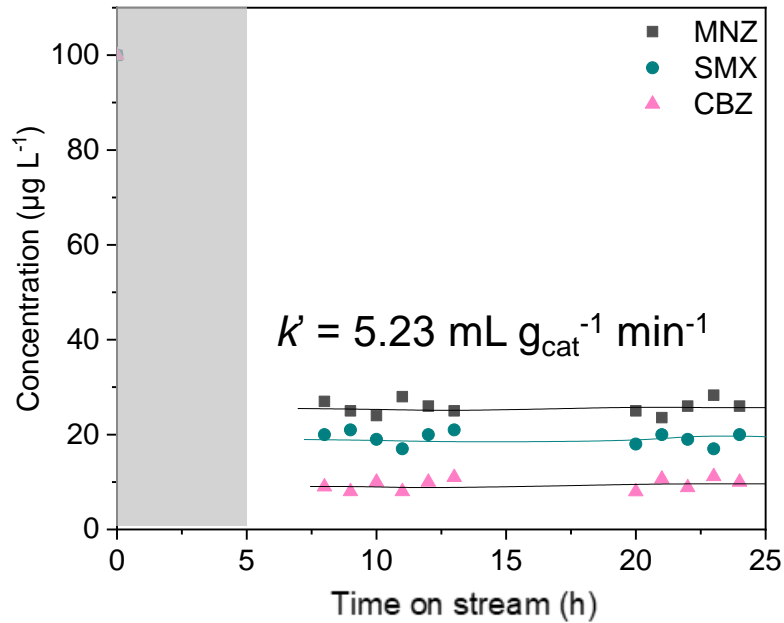
Q = 0.2 mL min⁻¹



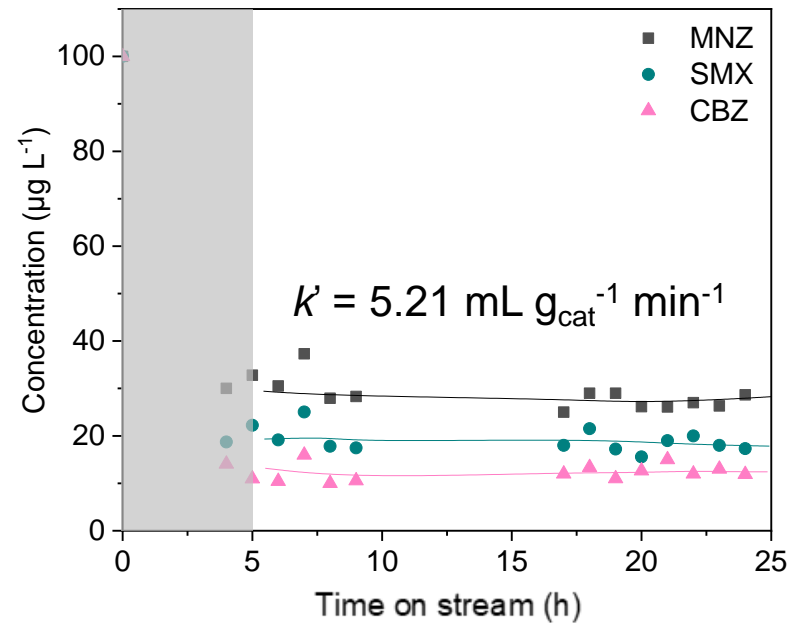
↑ Flow rate → ↓ Conversion

EFFECT H₂O₂ – Fe/Al₂O₃ foam

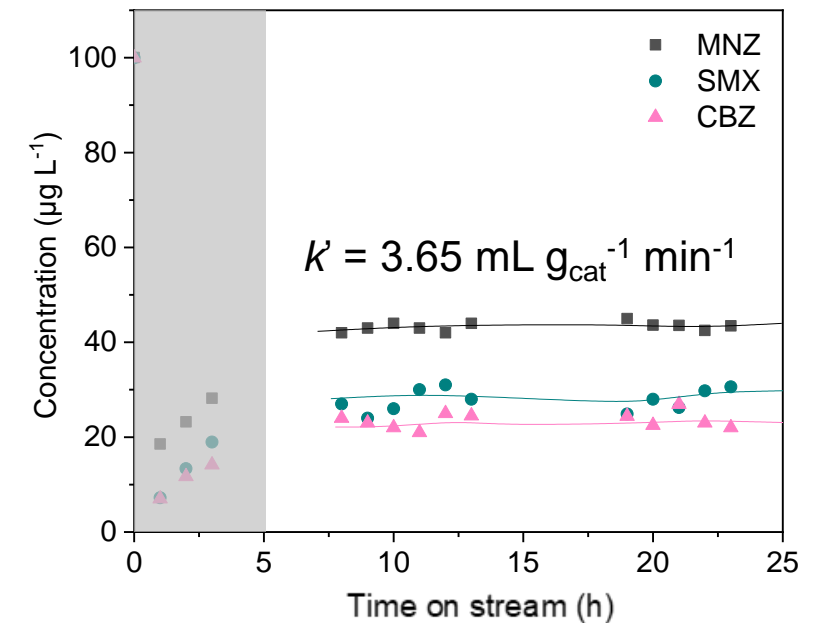
[H₂O₂] = 0.75 mg L⁻¹



[H₂O₂] = 1.49 mg L⁻¹

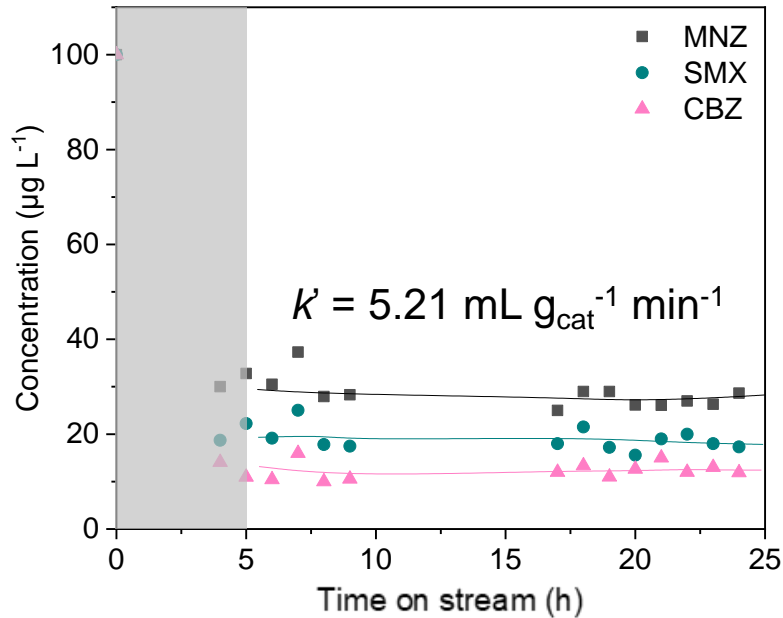


[H₂O₂] = 2.98 mg L⁻¹

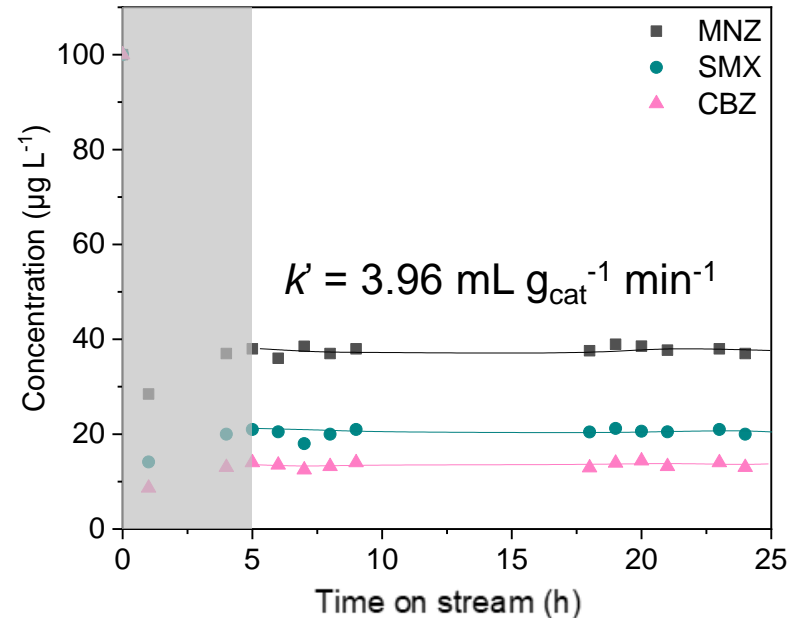


EFFECT of ORGANIC MATTER – Fe/Al₂O₃ foam

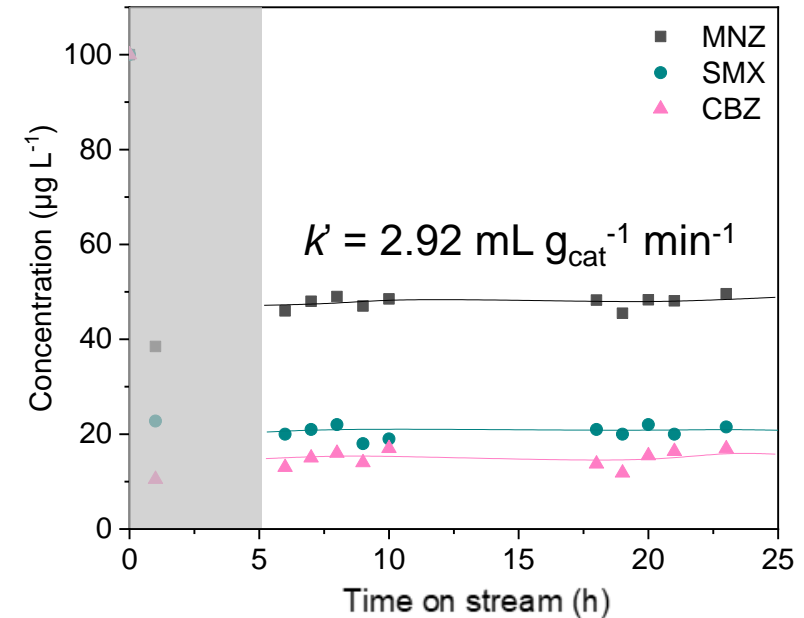
Deionized water







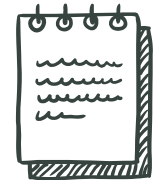
[NOM] = 1 mg L⁻¹



[NOM] = 5 mg L⁻¹



-  Structured foam catalysts were prepared by the coating with an active phase of iron oxide of Al_2O_3 , SiC and ZrO_2 supports, showing an adequate homogeneity.
-  Fe/ Al_2O_3 and Fe/SiC catalysts, were active for the degradation of three pharmaceuticals (MNZ, SMX and CBZ) upon a continuous Fenton reaction up to 200 h, exhibiting a notably catalyst stability.
-  The decrease of the feed flow led to higher activities and demonstrate the absence of mass transfer limitations.
-  The presence of NOM in the reaction medium showed a positive stability and just a slight decrease in the MNZ reactivity was obtained, demonstrating the versatility of the system.



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