



Perovskite $\text{LaMn}_x\text{Cu}_{1-x}\text{O}_3$ materials for heterogeneous electro-Fenton process

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Wastewater treatment problems

Water quality spoilage is been a worrying issue around the world in recent years due to human activities and climate change.

UNO 

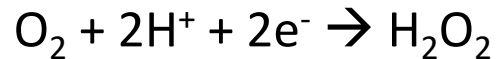


New technologies are necessary to treat wastewater effluents in a more effective and efficient way



Electro Fenton Heterogeneous Electro Fenton

REACTIONS IN THE CATHODE



FENTON-LIKE REACTIONS



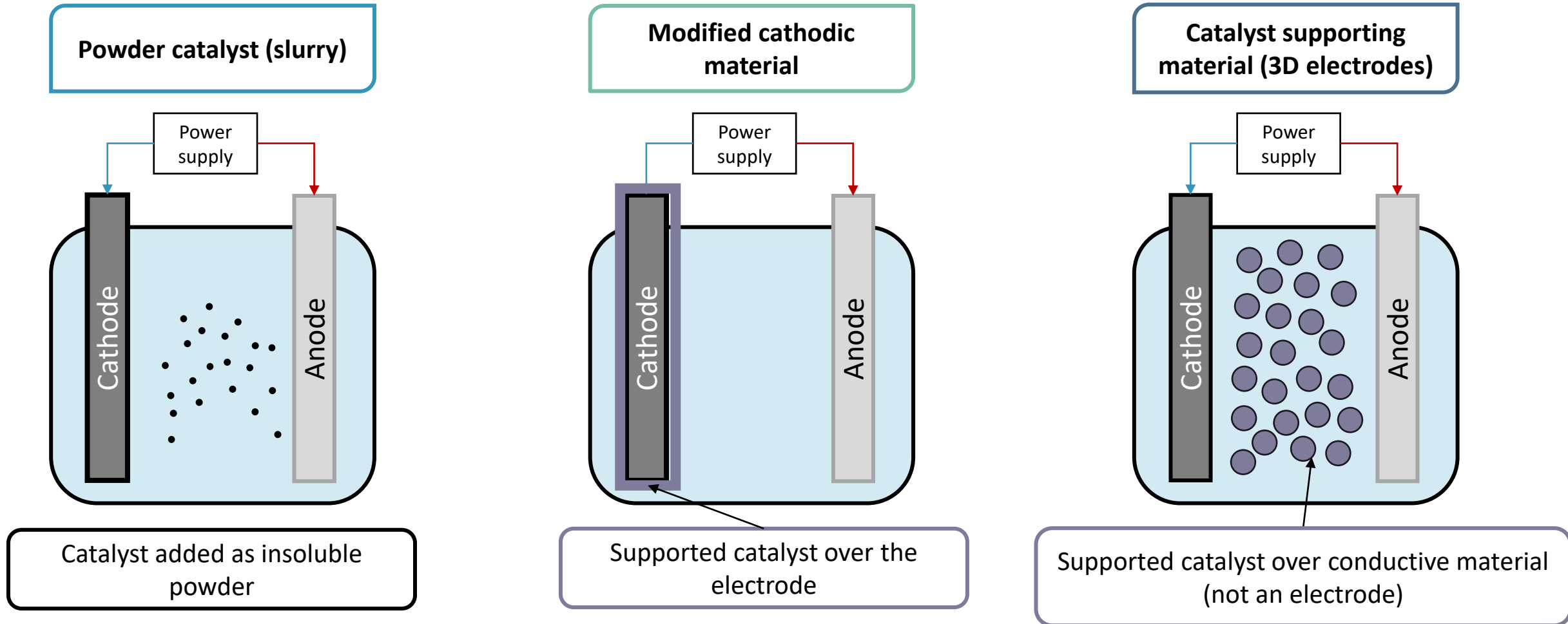
ADVANTAGES

- Possible neutral pH working.
- Easy separation, reusability and recyclability of the catalyst.
- The on-site production of H_2O_2 .
- Continuous regeneration of Fe^{2+} at the cathode.
- Easy automation.





Heterogeneous Electro Fenton Process: System configuration





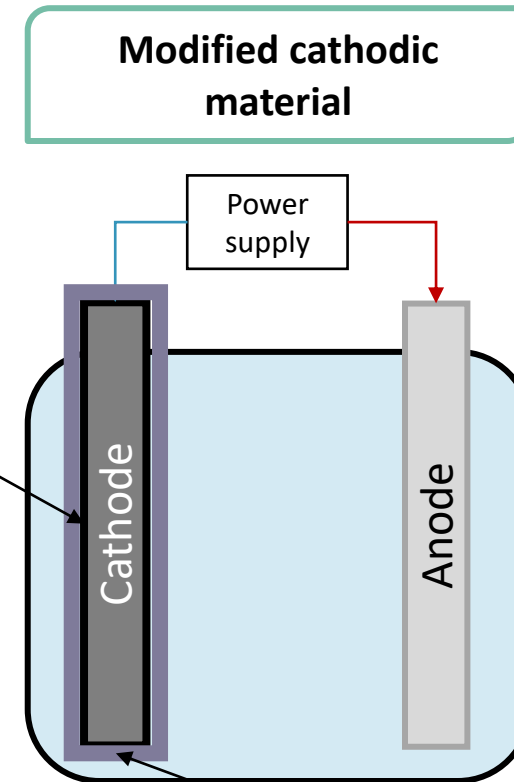
Heterogeneous Electro Fenton Process: System configuration

This type of deposition it could use in different type of cathodes, like **carbonaceous electrode**.



ADVANTAGES

- *In-situ* production of large quantities of H_2O_2
- Good electronic conductivity
- Mechanical and chemical stability
- High surface areas and porosity
- Excellent electrolytic efficiency at relatively low cost

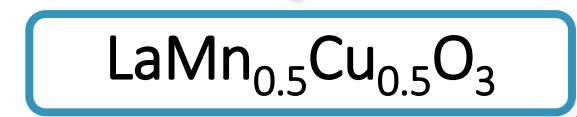
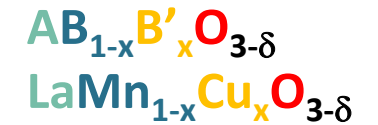
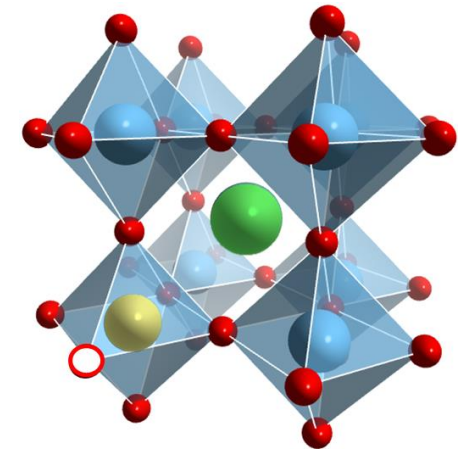
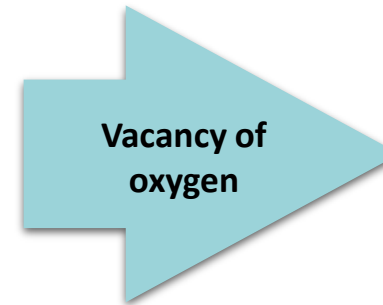
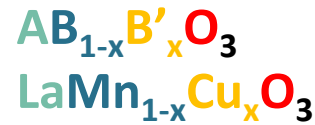
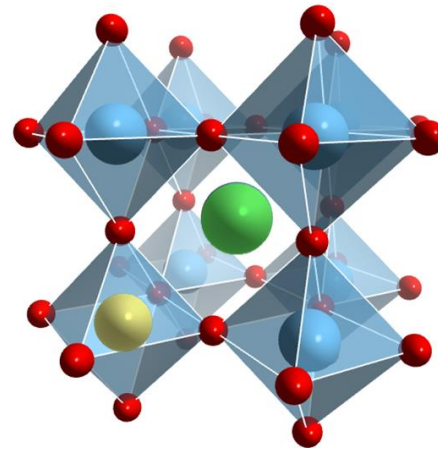
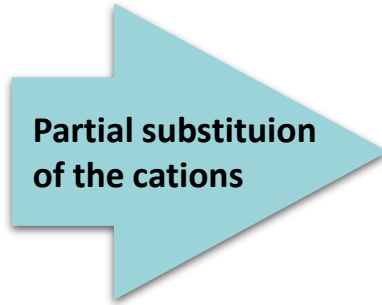
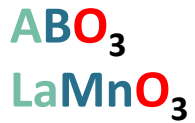
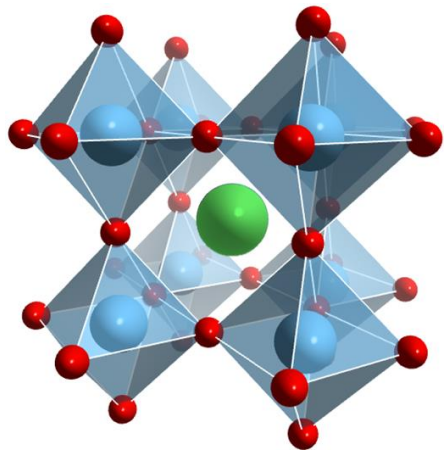




Catalyst: Perovskite

Estructure type ABO_3

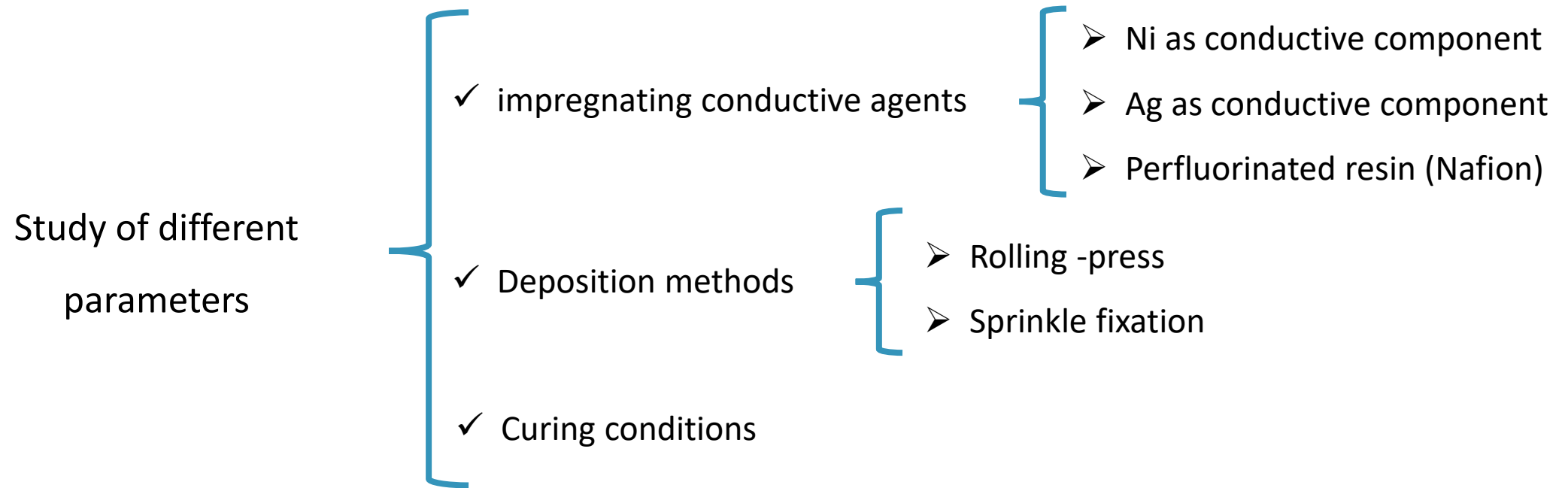
- **A:** Rare earth or alkaline earth metals (La, Sr...)
- **B:** transition metals (Cu, Fe, Mn, ...)



A.Cruz del Álamo, et al. *Catalysis Today* 361 (2021) 159–16



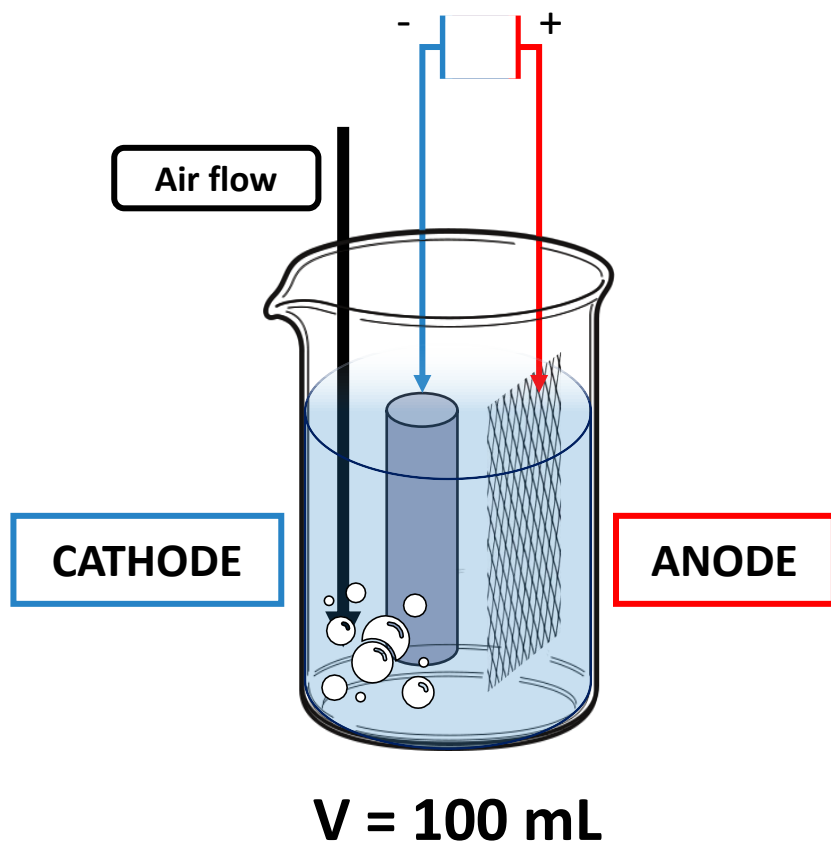
- Study and assessment of different deposition method of $\text{LaMn}_{0.5}\text{Cu}_{0.5}\text{O}_3$ catalyst over the cathode (working electrode) for degradation of **methylene blue (MB)** by heterogeneous electro Fenton process.





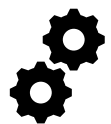
Electro Fenton experimental set-up

Galvanostatic conditions



Cathode Surface (graphite bar)	3	cm ²
Anode Surface (Ti/Pt metal rack)	6	cm ²
Distance between electrodes	2.5	cm
Intensity	15	mA
Current density	5	mA/cm ²
Reactor volume	100	mL
Pollutant [Methylene blue] ₀	50	mg/L
pH	6 ± 0.2	
Na ₂ SO ₄	50	mM
Air flow	300	mL/min
Stirring	600	rpm





Perovskite $\text{LaMn}_{0.5}\text{Cu}_{0.5}\text{O}_3$ synthesis

Perovskite material was prepared using a modified sol-gel citrated method, using citric acid as quelant agent

Mix of precursors 2h

Drying 70 °C 24h

Drying 110 °C 24h

Calcine 700 °C 5h

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Perovskite precursors:

- $\text{La}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$
- $\text{Mn}(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O}$
- $\text{Cu}(\text{CH}_3\text{COO})_2 \cdot 2\text{H}_2\text{O}$

Characterization

- X-Ray Diffraction (XRD)
- Nitrogen adsorption/desorption





Deposition of perovskite catalyst $\text{LaMn}_{0.5}\text{Cu}_{0.5}\text{O}_3$ over carbon graphite bar cathode

IMPREGNATING ELECTRIC CONDUCTIVE AGENTS

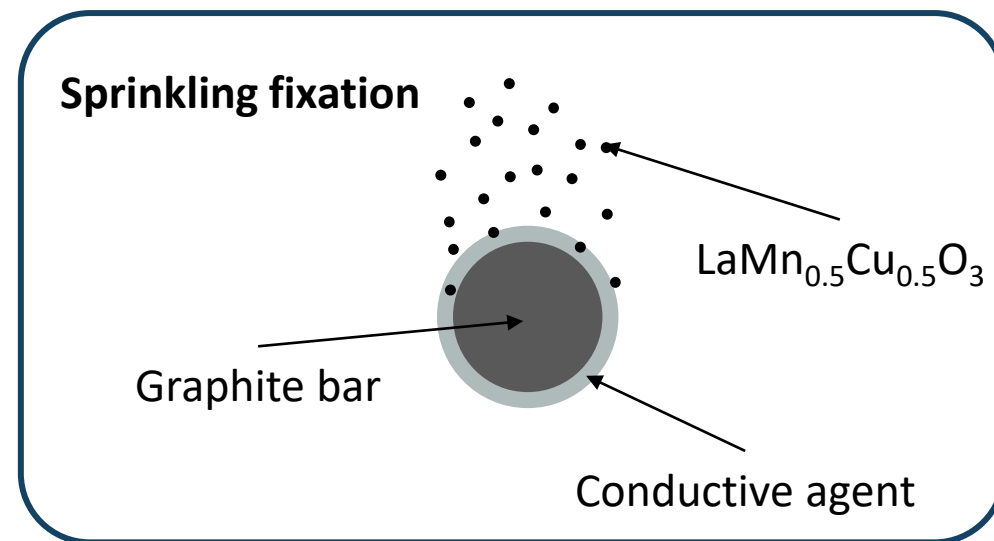
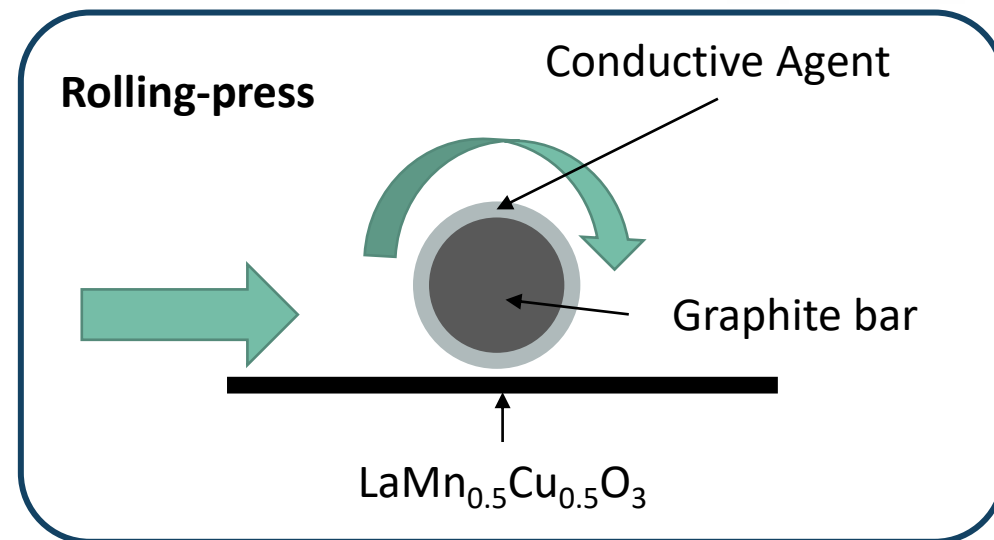
- **Nickel Filled Polymer (Chemtronic CW 2000):**
 - ✓ Nickel ≥ 50 - ≤ 75
 - ✓ 2-methoxy-1-methylethyl acetate ≥ 10 - ≤ 25
 - ✓ 2-butoxyethyl acetate ≥ 10 - ≤ 18
 - ✓ n-butyl acetate ≥ 10 - < 20
 - **Recommended curing conditions**
 - ✓ 15 to 20 minutes at room temperature
 - ✓ 10 - 15 minutes at 80 to 100°C
- **Silver filled polymer (Loctite Edag 5915):**
 - ✓ Ag content is not detailed by the supplier
 - ✓ Epoxy resin
 - **Recommended curing conditions**
 - ✓ 15 minutes @ 130°C
 - ✓ 10 minutes @ 177°C
- **Perfluorinated resin solution containing Nafion (5% w/w)**
 - ✓ 5 wt. % in lower aliphatic alcohols and water
 - ✓ 15-20 % water





Deposition Method

- 1- Application of electric conductive agents on the electrode surface
- 2- Deposition of powder perovskite catalyst
 - 2.1. Impregnation by **rolling** of the graphite bar over a perovskite powder bed
 - 2.2. **Sprinkling** of powder perovskite catalyst over the graphite bar
- 3- Curing conditions





Curing conditions

- Nickel Filled Polymer Chemtronic CW 2000

- ✓ Rolling Room temperatura cure (**Ni-R@RT**)
- ✓ Rolling 100°C cure (**Ni-R@100**)

- Silver filled polymer (Loctite Edag 5915)

- ✓ Rolling 130°C cure (**Ag-R@130**)
- ✓ Sprinkle 130°C cure (**Ag-S@130**)
- ✓ Rolling 177°C cure (**Ag-R@177**)

- Perfluorinated resin solution containing Nafion (5% w/w)

- ✓ Rolling 80 °C cure (**Nafion-R@80**)

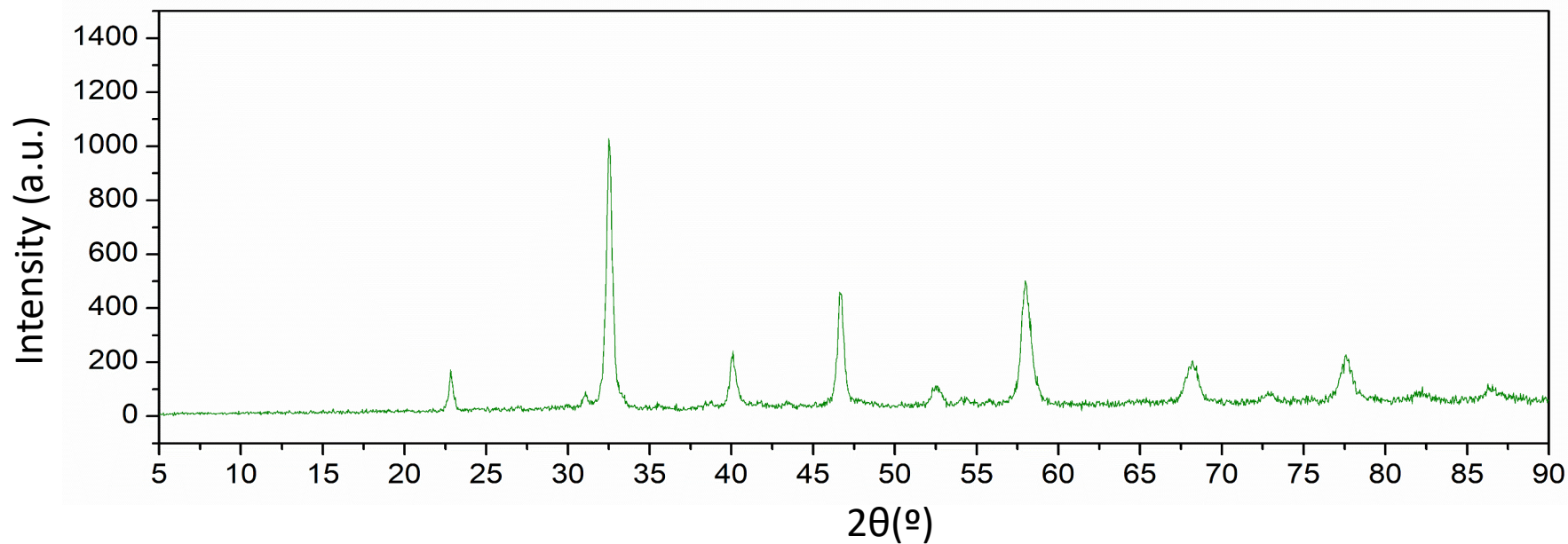
Modified electrodes were immersed in water under the same hydrodynamics conditions that used in the EF catalytic runs for 1 h (air bubbling, 300 ml/min but non-voltage potential) as washing and non-attached particles removal



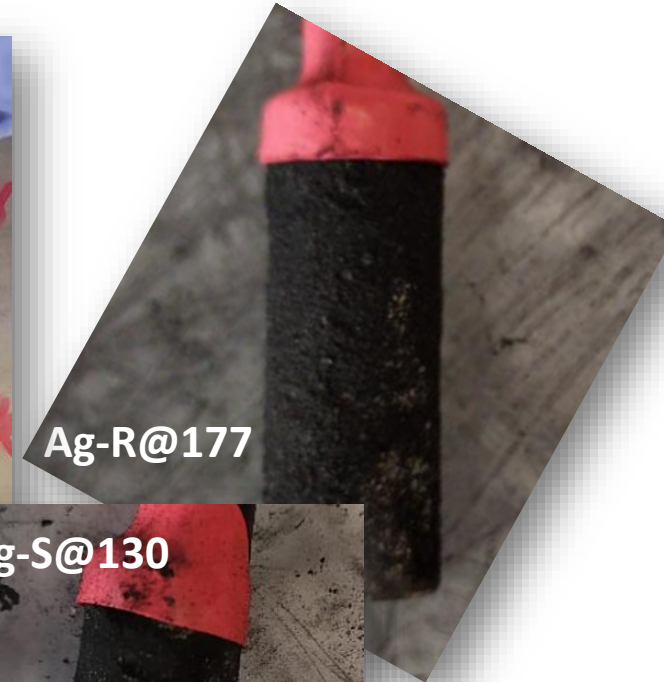
Catalyst Characterization

Characterization of perovskite $\text{LaMn}_{0.5}\text{Cu}_{0.5}\text{O}_3$

Perovskite materials	La: xMn: yCu: zCitric acid	BET Surface area (m_2/g)
$\text{LaMn}_{0.5}\text{Cu}_{0.5}\text{O}_3$	1: 0.5: 0.5: 0.3	3.68 ± 0.16



Deposition of perovskite catalyst $\text{LaMn}_{0.5}\text{Cu}_{0.5}\text{O}_3$ over carbon graphite bar cathode



Influence of different conductive agents

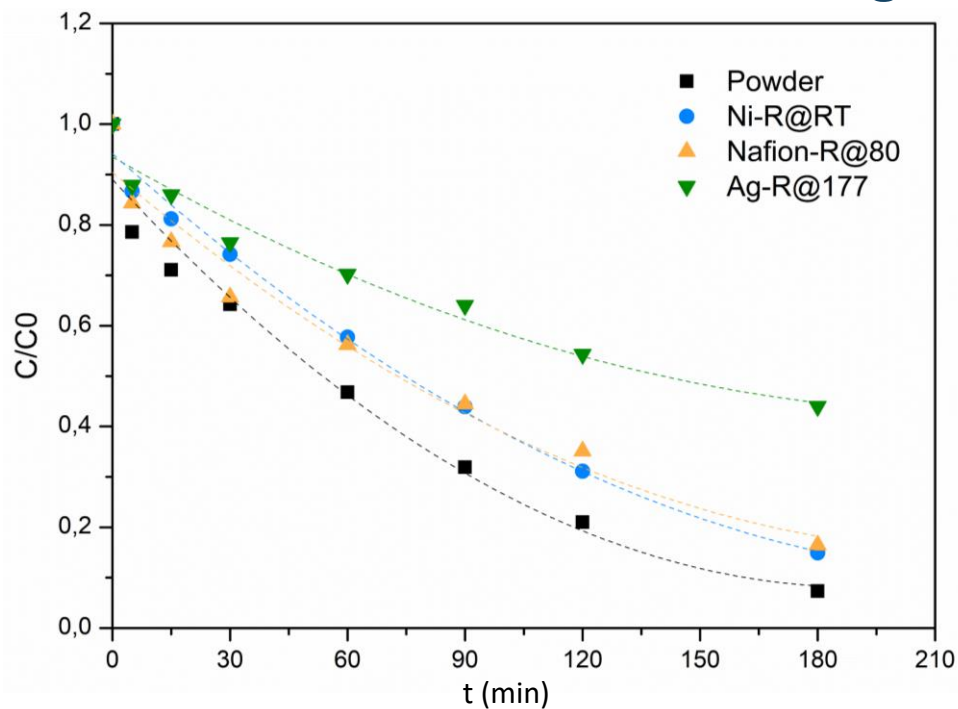
Perovskite content and losses

Perovskite-modified electrode	Perovskite content after curing conditions (mg)*	Perovskite content after immersion in water (1h)*	Perovskite loss after immersion in water (%)
Ni-R@RT	143.5	115.4	19.6
Ni-R@100	175.0	106.5	39.1
Ag-R@130	183.5	172.0	6.3
Ag-S@130	146.4	139.0	4.9
Ag-R@177	147.9	147.9	< 0.01
Nafion-R@80	203.9	163.3	19.9

*Perovskite mass over 3 cm² of cathode surface



Influence of different conductive agents: Comparison



- **Ni-R@100:** High MB removal, less perovskite loading.
- **Ag-R@177:** The lowest MB removal, major perovskite loading.
- **Nafion-R@80:** Similar MB removal than Ni-R@100; similar amount of perovskite than powder catalyst reaction

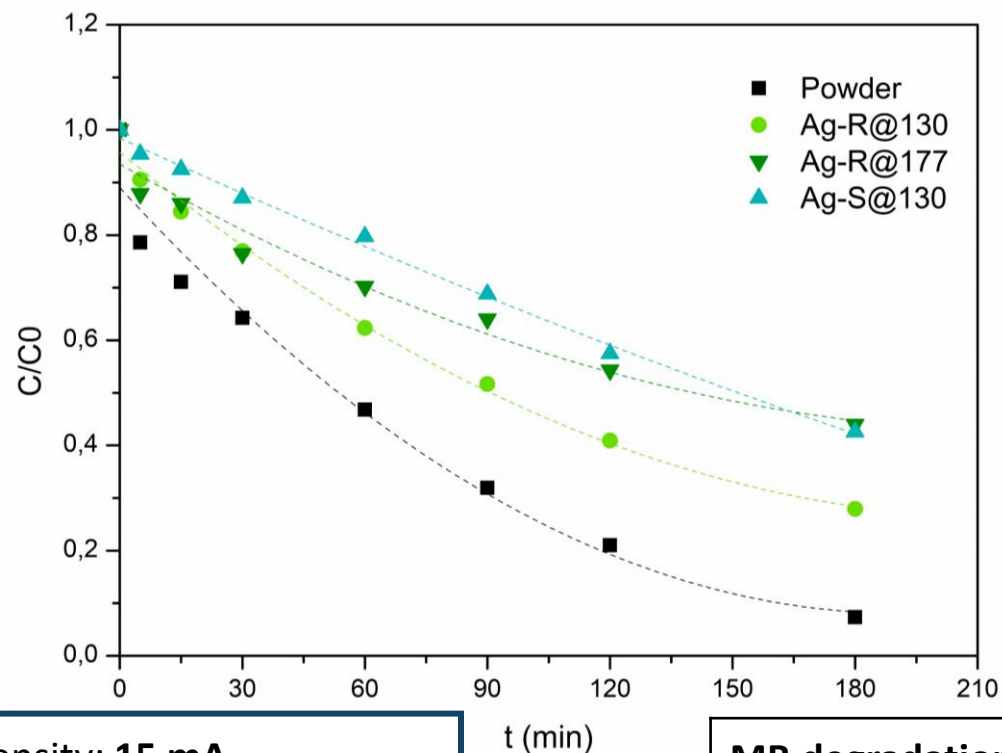
Presence of perfluorinated resin

- Intensity: **15 mA**
- Current density: **5 mA/cm²**
- Air Flow: **300 mL/min**
- Initial MB: **50 ppm**
- pH = **6 ± 0.2**
- Reactor volumen: **100 mL**

Perovskite (mg)	MB degradation (mg/L)					TOC (%)	Perovskite losses (%)	
	30'	60'	90'	120'	180'			
Ni-R@RT	1.1	31.2	24.2	18.5	13.1	6.4	31.3	0.3
Ag-R@177	1.5	33.9	31.1	28.3	24.1	19.5	NA	0.3
Nafion-R@80	1.6	30.9	26.5	21.0	16.6	7.8	37.5	0.1
Powder	1.9	31.6	23.0	15.7	10.3	3.6	39.6	--



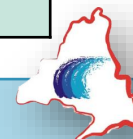
Influence of different conductive agents: cure conditions - deposition method



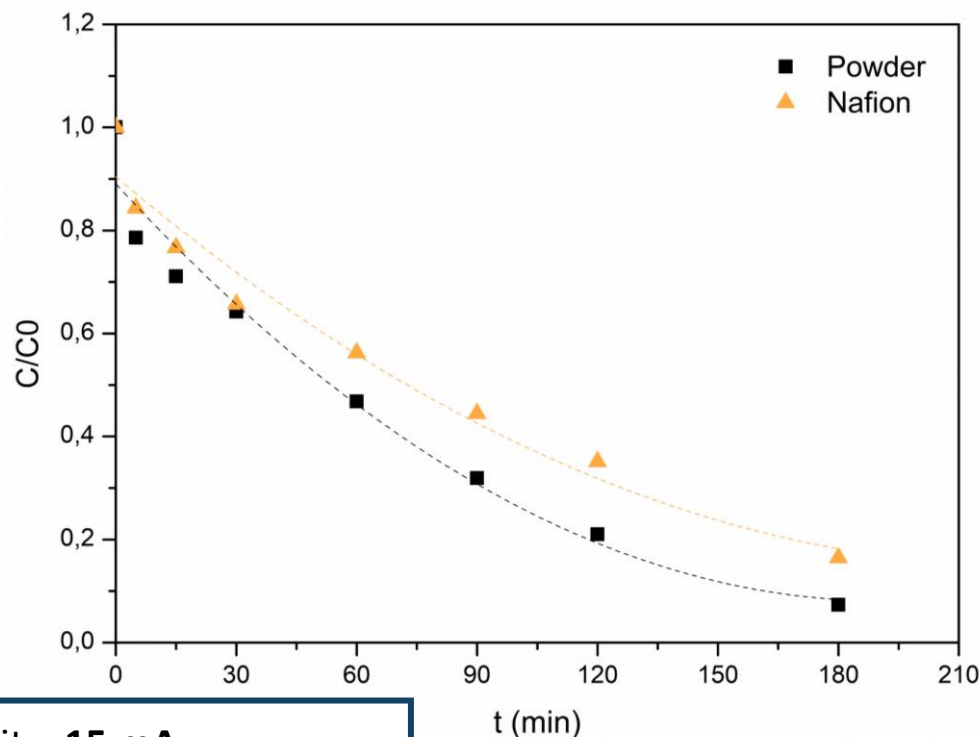
- Intensity: **15 mA**
- Current density: **5 mA/cm²**
- Air Flow: **300 mL/min**
- Initial MB: **50 ppm**
- pH = **6 ± 0.2**
- Reactor volumen: **100 mL**

- Ag conductive agent the best adherence. The catalyst losses after washing the lowest registered.
- Catalytic activity of these depositions are lower despite the amount of perovskite over the cathode
- Free surface in contact with oxygenated liquid medium is a key parameter

	Powder	Ag-R@130	Ag-S@130	Ag-R@177
MB degradation (%)	92.7	72.0	57.4	56.0
Catalyst concentration (g/L)	1.9	1.7	1.4	1.5
Perovskite loss after EF reaction (%)	--	1	0.04	0.3



Influence of different conductive agents: deposition method



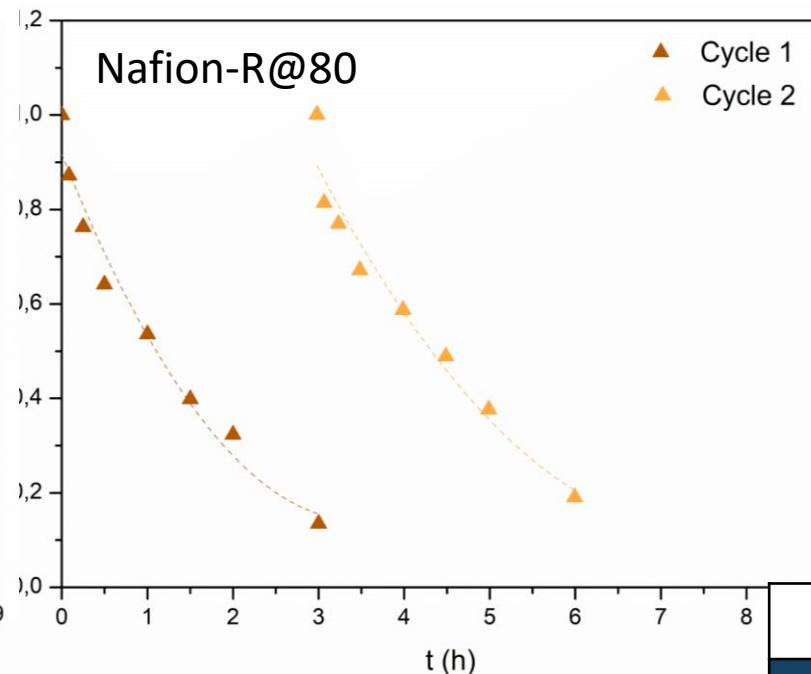
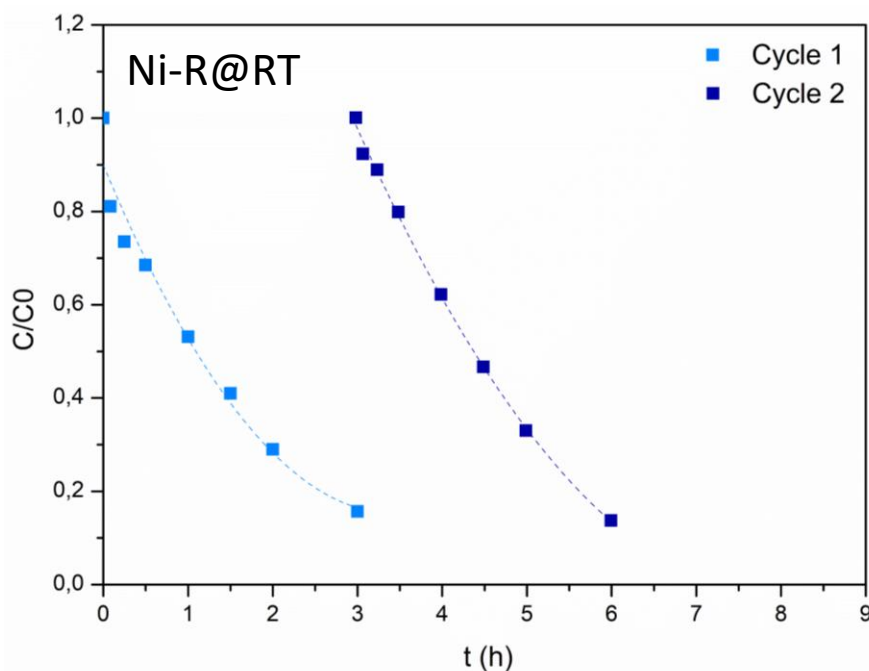
- Intensity: **15 mA**
- Current density: **5 mA/cm²**
- Air Flow: **300 mL/min**
- Initial MB: **50 ppm**
- pH = **6 ± 0.2**
- Reactor volumen: **100 mL**

- **Nafion-R@80**: MB degradation similar than powder reactions.
- Perovskite deposited is quite like powder catalyst reaction. The lowest losses of perovskite after reaction of all method tested.
- Conductivity due to perfluorinated resin enhance degradation of MB

	Powder	Nafion-R@80
MB degradation (%)	92.7	83.5
TOC degradation (%)	39.6	37.5
Catalyst concentration (g/L)	1.9	1.6
Perovskite losses after reaction (%)	--	0.1



Catalyst reuse with Ni and Nafion conductive agent



- Intensity: **15 mA**
- Current density: **5 mA/cm²**
- Air Flow: **300 mL/min**
- Initial MB: **50 ppm**
- pH = **6 ± 0.2**
- Reactor volumen: **100 mL**

Reused catalyst over Ni-R@RT and Nafion-R@80 retains the catalytic activity as efficient as the fresh one during 2 cycles

	Ni-R@RT		Nafion-R@80	
	Cycle 1	Cycle 2	Cycle 1	Cycle 2
MB degradation (%)	84.3	85.9	86.6	80.6
TOC degradation (%)	28.8	33.8	31.9	43.1
Catalyst (g/L)	1.2	1.2	1.6	1.6
Perovskite losses after reaction (%)	0.3	0.3	0.12	< 0.01



Deposition of $\text{LaMn}_{0.5}\text{Cu}_{0.5}\text{O}_3$ over carbon graphite bar cathode

- Results show higher perovskite loading in the cathode reduces the activity of the EF process, suggesting the graphite surface is less effective for the reduction of oxygen to form hydrogen peroxide by a higher covering of the perovskite particles.
- The immobilization of perovskite by the perfluorosulphonic Nafion resin is very active despite the high perovskite loading, probably due to the better conductivity of the perfluorosulphonic polymer
- Both, Sprinkle and Rolling method, and cure temperature present the same effectivity for deposition of catalyst over the electrode.
- The reusability of the catalyst, on Ni-R@RT and Nafion-R@80, shows to retain the catalytic activity as efficient as the fresh one during 2 cycles.





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